

gr. HI – 17 – 5i ,  
HI – 17 – 4i

2021 y.

**Calculation task № 15 (individual) Example .**  
**(INDIVIDUAL – DIFFERENT VARIANTS in the table)**

Determine the flow capacity of the gathering line if its length is 9360 m; the diameter is 120 mm, pressure at the wellhead (inlet pressure) is 14.2 MPa; gas treatment unit inlet pressure (pressure at the end of the gathering line) is 13 MPa; absolute density of gas at standard conditions is 0.79 kg/m<sup>3</sup>; inlet temperature is 306 K; temperature at the end of the gathering line is 301 K; coefficient of hydraulic resistance of the pipes is 0.023. Coefficient of decrease of the flow capacity of the gathering line is 0.9 (production of the well is gas with liquid).

Determine average gas compressibility factor (at average pressure and average temperature in the gathering line) by means of empirical formula.

$$P_1 = 14.2 \quad \text{MPa}$$

$$P_2 = 13 \quad \text{MPa}$$

$$L = 9360 \quad \text{m}$$

$$d_{\text{in}} = 120 \quad \text{mm}$$

$$\lambda = 0.023$$

$$\rho_{\text{g.}} = 0.79 \quad \frac{\text{kg}}{\text{m}^3}$$

$$T_1 = 306 \quad \text{K}$$

$$T_2 = 301 \quad \text{K}$$

$$E_d = 0.9$$

Determine : the flow capacity of the gathering line

$$Q_g \quad - \quad ?$$

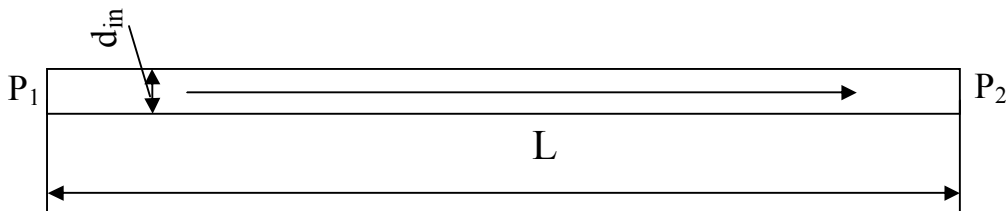
**Solution**

The flow capacity of the gathering line :

$$Q_g = 103.15 \cdot E_d \sqrt{\frac{(P_1^2 - P_2^2) \cdot d_{\text{in}}^5}{\lambda \cdot \rho_{\text{g.r.}} \cdot Z_{\text{avr}} \cdot T_{\text{avr}} \cdot L}} \quad (1)$$

**Explanation to the formula (1) :**

$Q_g$  is the flow capacity of the gathering line, **m<sup>3</sup>/day**;  $d_{in}$  is inner diameter of the gathering line, **cm**;  $P_1$  is the pressure at the beginning of the gathering line (pressure at the inlet of the gathering line), **atm.**;  $P_2$  is the pressure at the end of the gathering line (pressure at the outlet of the gathering line), **atm.**;  $E_d$  is the coefficient of the decrease of the flow capacity of the gathering line, without units (  $E_d = 1$  or sometimes  $E_d = 0.8 - 0.95$ ), according to the data of calculation task  $E_d = 0.9$ ;  $L$  is the length of the gathering line, **km**;  $\lambda$  is coefficient of hydraulic resistance of the pipes, without units;  $Z_{avr}$  is gas compressibility factor (at average pressure and average temperature in the gathering line), without units;  $\rho_{g.r.}$  is relative density of gas, without units;  $T_{avr}$  is the average temperature in gathering line, **K**.

**Figure.**

Relative density of gas

$$\rho_{g.r.} = \frac{\rho_g}{\rho_{air.st.}} \text{ where } \rho_{air.st.} = 1.205 \text{ kg/m}^3 \text{ is the density of air at standard conditions (standard pressure } P_{atm} = 0.1 \text{ MPa, standard temperature } T_{st} = 293 \text{ K).}$$

$$\rho_{g.r.} = \frac{0.79}{1.205} = 0.6556$$

Gas compressibility factor  $Z_{avr}$  :

$$Z_{avr} = (0.4 \cdot \log(T_{red.avr.}) + 0.73)^{P_{red.avr.}} + 0.1 \cdot P_{red.avr.} \quad (2)$$

$T_{red.s.}$  is reduced temperature of gas, without units;  $P_{red.s.}$  is reduced pressure of gas, without units.

$$P_{\text{red.avr.}} = \frac{P_{\text{avr.}}}{P_{\text{cr.}}} \quad ; \quad T_{\text{red.avr.}} = \frac{T_{\text{avr.}}}{T_{\text{cr.}}}$$

where  $P_{\text{cr.}}$  is critical pressure of gas, MPa;  $T_{\text{cr.}}$  is critical temperature of gas, K.

$$P_{\text{cr.}} = 4.892 - 0.4048 \cdot \rho_{\text{g.r.}} \quad , \text{ MPa.}$$

$$T_{\text{cr.}} = 170.8 \cdot \rho_{\text{g.r.}} + 94.717 \quad , \text{ K.}$$

$$P_{\text{cr.}} = 4.892 - 0.4048 \cdot 0.6556 = 4.627 \text{ MPa.}$$

$$T_{\text{cr.}} = 170.8 \cdot 0.6556 + 94.717 = 206.69 \text{ K}$$

We have to determine average pressure and average temperature in the gathering line.

Average pressure in the gathering line :

$$P_{\text{avr.}} = \frac{2}{3} \left( P_1 + \frac{P_2^2}{P_1 + P_2} \right) \quad P_{\text{avr.}} = \frac{2}{3} \left( 14.2 + \frac{13^2}{14.2 + 13} \right) = 13.61 \text{ MPa}$$

Average temperature in the gathering line :

$$T_{\text{avr.}} = \frac{T_1 - T_2}{\ln \left( \frac{T_1}{T_2} \right)} \quad T_{\text{avr.}} = \frac{306 - 301}{\ln \left( \frac{306}{301} \right)} = 303.49 \text{ K}$$

Reduced pressure of gas and reduced temperature of gas :

$$P_{\text{red.avr.}} = \frac{P_{\text{avr.}}}{P_{\text{cr.}}} = \frac{13.61}{4.627} = 2.941$$

$$T_{\text{red.avr.}} = \frac{T_{\text{avr.}}}{T_{\text{cr.}}} = \frac{303.49}{206.69} = 1.468$$

$$Z_{avr} = (0.4 \cdot \log(T_{red.avr.}) + 0.73)^{P_{red.avr.}} + 0.1 \cdot P_{red.avr.} =$$

$$= (0.4 \cdot \log(1.468) + 0.73)^{2.941} + 0.1 \cdot 2.941 = 0.807$$

It is very important to remember that into the formula (1), that is formula for determination of the flow capacity of the gathering line we put :  $P_1$  and  $P_2$  in **atm.**,  $d_{in}$  – in **cm**,  $L$  – in **km** and then we get  $Q_g$  in **m<sup>3</sup>/day**.

### Conversion of units :

$$P_1 = P_1 \cdot 10 = 14.2 \cdot 10 = 142 \text{ atm} ; \quad P_2 = P_2 \cdot 10 = 13 \cdot 10 = 130 \text{ atm} ;$$

$$L = 9.36 \text{ km} ; \quad d_{in} = 12 \text{ cm} .$$

Calculation of the flow capacity of the gathering line :

$$Q_g = 103.15 \cdot 0.9 \sqrt{\frac{(142^2 - 130^2) \cdot 12^5}{0.023 \cdot 0.6556 \cdot 0.807 \cdot 303.49 \cdot 9.36}} = 446.06 \times 10^3 \frac{\text{m}^3}{\text{day}} =$$

$$= 446.06 \frac{\text{thm}^3}{\text{day}}$$

$$\text{Answer : } Q_r = 446.06 \frac{\text{thm}^3}{\text{day}}$$